

High Efficiency Cross-Flow Microsand Filtration as Pretreatment in Desalination Applications

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# Background

- There has been much effort in energy reduction of main desalting step in seawater desalination.
- This study proposes to use a high efficiency cross-flow microsand filtration in the pre-treatment step.
- Current Seawater Desalination Pretreatment Process:



• Seawater Pretreatment with VAF and Vortisand:



• A typical traditional pre-treatment system would require 0.3-0.4kwh/m3, while a fine filtration system only requires about 1-2 bar pressure drop, which is equivalent to around 0.1-0.2kwh/m3



### Process design: Feed water key characteristics

- Feed water:
  - Coarse screen filtered seawater from Tuas South Desalination Plant
  - TDS 31 34,000 ppm
  - Temperature 30 33'C,
  - pH 7.8-8.4
  - TSS 5-20mg/L
  - Turbidity 3 15 NTU



#### Process design: Feed water key characteristics

- Laser particle size distribution results show that the majority of the particles are submicron in size.
- High efficiency sand filters are able to filter up to sub-micron level, simple to operate and require simple cleaning steps, thus is the technology chosen to be tested for seawater pre-treatment.

	Particle Size (µm)	Differential Result							
		Unit : counts/mL				Unit : % counts			
		Data 1	Data 2	Data 3	Average	Data 1	Data 2	Data 3	Average
	0.5	504060	503310	505040	504137	92	92	92	92
7th Apr 2021	1	43810	44030	43950	43930	8	8	8	8
Seawater sample	10	690	680	780	717	<1	<1	<1	<1
	20	70	20	10	33	<1	<1	<1	<1
	25	10	10	10	10	<1	<1	<1	<1
	30	10	30	10	17	<1	<1	<1	<1
	50	<1	<1	<1	<1	<1	<1	<1	<1
evoqua	80	<1	<1	<1	<1	<1	<1	<1	<1



- Cross-flow microsand filtration enables much higher performance than traditional multimedia filters.
- MMF uses different layers of media for filtration.
  - Utilises depth filtration (300-700µm), 5-10 gpm/ft<sup>2</sup>.
  - Requires higher backwash flowrate to achieve fluidisation of sand & anthracite. Roughly twice the filtration flowrate.
  - Only able to achieve **10 to 25-micron filtration**.





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  - Only able to achieve **10 to 25-micron filtration**.
- Vortisand® HE cross-flow microsand(150µm) filtration.
  - Combines suspension & depth filtration, 20 gpm/ft<sup>2</sup> (4X)
  - Requires much lower backwash flowrate **40% of filtration flowrate**.
  - Able to achieve submicron filtration, SDI <5.





• Cross-flow device keeps solids continuously in suspension instead of pushing it into the sand and quickly plugging the media.







• Possibility to stack vessels for halving already compact footprint.







#### Particle count results, selection of guard-filter

- Raw seawater feed is from 2mm travelling screen filter, so a prefilter for the Vortisand® is needed.
- Two stages of V-series<sup>™</sup> self-cleaning screen filters with 25 and 10-micron screen sizes were installed for flexibility in testing different running options.

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### Evoqua's V-series<sup>™</sup> self-cleaning screen filter

- Most self-cleaning filters on the market uses piston or motor type mechanism.
- V-series<sup>™</sup> filters utilises a reverser & pawl design to generate an efficient cleaning path of the suction nozzles.
- The self-cleaning function is activated by just opening a flush valve and the system pressure provides the motive force for the whole mechanism.
- Only instrumentation is a flush valve & DP switch.





### Process Design – Final Design

• Jar testing was performed to choose a suitable coagulant, FeCl<sub>3</sub>.





#### Test Results – Lab readings



#### Test Results – Onsite readings



# Process Improvement: FeCl<sub>3</sub> & Backwash duration auto-calculation

- Initially the FeCl<sub>3</sub> dosage and backwash duration was manually controlled.
- After collection of several data points, FeCl<sub>3</sub> auto dosing and backwash duration calculation vs. feed turbidity was implemented and continually finetuned.





#### Vortisand® maintenance regime

- Operation: ~30 to 40 minutes runtime
- Cleaning with sodium hypochlorite once a week @ ~185ppm free chlorine "in the vessel" (with no free chlorine dosing upstream).
- Once a month HCl cleaning @ pH <3, 1hr soak



#### Challenges encountered

- If an incoming high turbidity/algae bloom incident occurs, damages to sand unrecoverable.
  - Implemented incoming turbidity limit trip @ 18NTU.

- Preferably require DAF before Vortisand®, which also can't take oil & grease in the event of oil-spill incidents in Singapore waters.





- Sampling solenoid turbidity valves cause erratic reading
  - Implemented turbidity analyser back-pressure control.



# Comparison of Vortisand® and UF

WATER TECHNOLOGIES

Description	Vortisand®	UF			
Design Flow rate	8-10 m <sup>3</sup> /h	10 m <sup>3</sup> /h			
Filtrate Turbidity	<0.2 NTU	<0.1 NTU			
Filtrate SDI	< 5, average 3	<3			
Energy Consumption	0.04 kWh/m3	0.13 kWh/m3			
Chemical Cleaning	Only to control bootorial growth when no	Acid/Caustic/Disinfectant:			
	disinfectant dosed upstream	<ul> <li>Chemical Enhanced Backwash ~ Daily/Weekly</li> <li>Cleaning In Place (with soak) ~ Weekly/Monthly</li> </ul>			
Cleaning chemicals	Biocide may be used during backwash if no continuous Sodium Hypochlorite dosing, acid cleaning may be used every 2-3 months if FeCl3 as coagulant	Chloric Acid (Or Sulfuric Acid), Sodium Hypochlorite, Citric Acid, Sodium Hydroxide			
Wastewater need neutralization?	Not required	Yes			
Media shelf life or membrane life	5 years (recommended)	3-5 years (typical)			
Recovery rate	~80% (When scale up, it could be up to 95%)	~90% (with air scouring) (Note: w/o air scouring, recovery can be lower)			

# **Backup Slides**



# SDI filter papers







#### THANK YOU

